

**MODELING AND SIMULATION OF THE BEER  
FERMENTATION PROCESS AND TEMPERATURE  
CONTROL**

Warnasooriya Mudiyansele Dilantha Rangana Warnasooriya

(07/8209)



Thesis submitted in partial fulfillment of the requirements for the degree Master of  
Science in Sustainable Process Development

Department of Chemical and Process Engineering

University of Moratuwa

Sri Lanka

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W.M.D.R. Warnasooriya

**Thesis Title** : Modeling and Simulation of the Beer Fermentation Process and Temperature Control

**Student Name:** W. M. D. R. Warnasooriya (07/8209)

“I have supervised and accepted this thesis/dissertation for the award of the degree”

Signature of the supervisor:

Date

.....

.....

Bernt Lie, Professor Ph.D./dr.ing.

Head of Department of Electrical Engineering,

Information Technology and Cybernetics,

Telemark University College,

P.O. Box 203/Postboks 203,N-3901 Porsgrunn,

Norway.

Signature of the co-supervisor:

Date

.....

.....

Dr. P.G. Rathnasiri,

Senior Lecturer,

Department of Chemical and Process Engineering,

University of Moratuwa,

Sri Lanka.

## **Dedication**

I dedicate this thesis for my parents and teachers, who have supported me all the way since the beginning of my studies.

Also, this thesis is dedicated to my fiancée who has been a great source of motivation and inspiration.



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## Abstract

Beer is the most common alcoholic drink around the world. When talking about the beer quality, flavor of the beer is more concerned. Most of the brewers in Sri Lanka are using traditional methods to brewing beer. Most of brewers using pre identified recipe to produce mass production of beer. Therefore, beer quality i.e. flavor is varying brand by brand. It is important to study the variation of temperature, how will affect to the final alcohol production and the flavor compound formation. Beer manufacturing industry can be used this knowledge to increase the production efficiency and the product quality.

It is very important to know about dynamics of forming flavor compounds. In this work the fermentation process is concerned since all the flavor compounds are formed during the fermentation. The mechanistic model is developed by based on the knowledge of biochemical processes in the yeast cell and previously developed mathematical models which are available in the literature. There are many beer models can be found such as Engasser et al.,(1981);Growth kinetic model, Gee at al.,(1988), Phisalaphong et al.(2006);Growth kinetic model and effect on temperature, W.F. Ramirez and J. Maciejowski.,(2007);Optimal beer fermentation, etc. The beer fermentation process is modeled and simulated in MATLAB/Simulink environment.

Growth model, nutrient model, and the flavor model are considered and developed. Growth model consists of sugar consumption, biomass growth and ethanol formation models. Those models are developed with temperature dependent parameters to observe the effect of the temperature. Three amino acids which are valine, leucine and iso leucine are considered for the Nutrient model. Consumption of these three amino acids is considered during fermentation. Flavor model is developed based on the growth model and the nutrient model. Flavor compounds are categorized into three groups which are fusel alcohols, esters and vicinal diketones. Altogether nine parameters are considered as flavor compounds and the effects of temperature on those are simulated with MATLAB/Simulink and JModelica. Industrial temperature profile is obtained and applied for the developed model and simulated in MATLAB/Simulink and the results are analyzed.

PI controller is applied to get identified temperature profile to obtain flavor formation and the dynamic model is used for find suitable controller parameters for the best control. The controller is simulated in MATLAB/Simulink.

Keywords: Beer, Fermentation, Flavor, Modeling, Simulation, Temperature, Control

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## Nomenclature

Symbol	Description
G	Glucose concentration (mol/m <sup>3</sup> )
M	Maltose concentration (mol/m <sup>3</sup> )
N	Maltotriose concentration (mol/m <sup>3</sup> )
X	Biomass concentration (mol/m <sup>3</sup> )
E	Ethanol concentration (mol/m <sup>3</sup> )
$\mu_1$	Specific rate of glucose uptake (h <sup>-1</sup> )
$\mu_2$	Specific rate of maltose uptake (h <sup>-1</sup> )
$\mu_3$	Specific rate of maltotriose uptake (h <sup>-1</sup> )
$\mu_X$	Specific rate of yeast growth (h <sup>-1</sup> )
$Y_{XG}$	Yield coefficient, mole X per Mole G
$Y_{XM}$	Yield coefficient, mole X per Mole M
$Y_{XN}$	Yield coefficient, mole X per Mole N
$X_0$	Initial yeast concentration (mol/m <sup>3</sup> )
$Y_{EG}$	Yield coefficient, mole E per Mole G
$Y_{EM}$	Yield coefficient, mole E per Mole M
$Y_{EN}$	Yield coefficient, mole E per Mole N
$K_x$	Empirical yeast growth inhibition constant (mol/m <sup>3</sup> ) <sup>2</sup>
$\mu_i$	Maximum reaction velocity for i <sup>th</sup> sugar ( i = G, M or N, h <sup>-1</sup> )
$K_i$	Michaelis constant for i <sup>th</sup> sugar ( i = G, M or N, mol/m <sup>3</sup> )
$K'_i$	Inhibition constant for i <sup>th</sup> sugar ( i = G or M, mol/m <sup>3</sup> )
$\mu_{i0}$	Arrhenius frequency factor for maximum velocity (h <sup>-1</sup> )
$K_{i0}$	Arrhenius frequency factor for michaelis constant (mol/m <sup>3</sup> )
$K'_{i0}$	Arrhenius frequency factor for inhibition constant (mol/m <sup>3</sup> )
$E_{\mu_i}$	Arrhenius activation energy for maximum velocity (cal/mol)
$E_{K_i}$	Arrhenius activation energy for michaelis constant (cal/mol)
$E_{\mu_i}$	Arrhenius activation energy for inhibition constant (cal/mol)



R	Gas constant (cal/mol K)
T	Temperature ( $^{\circ}\text{C}$ )
$\rho$	Density of wort ( kg/m <sup>3</sup> )
C <sub>p</sub>	Specific heat capacity of wort (kg/mol $^{\circ}\text{K}$ )
$\Delta H_{\text{FG}}$	Overall heat of formation for glucose ( J/mol)
$\Delta H_{\text{FM}}$	Overall heat of formation for maltose ( J/mol)
$\Delta H_{\text{FN}}$	Overall heat of formation for maltotriose ( J/mol)
$Y_{\text{LX}}$	Yield coefficient , moles leucine needs per mol biomass growth
$Y_{\text{IX}}$	Yield coefficient , moles isoleucine needs per mol biomass growth
$Y_{\text{VX}}$	Yield coefficient , moles valine needs per mol biomass growth
$K_{\text{L}}$	Michaelis constant for leucine (mol/m <sup>3</sup> )
$K_{\text{I}}$	Michaelis constant for isoleucine (mol/m <sup>3</sup> )
$K_{\text{V}}$	Michaelis constant for valine (mol/m <sup>3</sup> )
L	leucine concentration (mol/m <sup>3</sup> )
I	Isoleucine concentration (mol/m <sup>3</sup> )
V	Valine concentration (mol/m <sup>3</sup> )
D	First order time delay (h)
$\tau_{\text{d}}$	First order time constant for delay (h)
t	Time (h)
IB	Isobutyl alcohol concentration (mol/m <sup>3</sup> )
IA	Isoamyl alcohol concentration (mol/m <sup>3</sup> )
MB	2-methyl-1-butanol concentration (mol/m <sup>3</sup> )
P	n-propanol concentration (mol/m <sup>3</sup> )
$Y_{\text{IB}}$	Isobutyl alcohol yield
$Y_{\text{IA}}$	Isoamyl alcohol yield
$Y_{\text{MB}}$	2-methyl-1-butanol alcohol yield
$Y_{\text{PE}}$	n-propanol alcohol yield
$\mu_{\text{V}}$	Specific rate of valine uptake ( $\text{h}^{-1}$ )
$\mu_{\text{L}}$	Specific rate of leucine uptake ( $\text{h}^{-1}$ )
$\mu_{\text{I}}$	Specific rate of isoleucine uptake ( $\text{h}^{-1}$ )
EA	Ethyl acetate concentration (mol/m <sup>3</sup> )
EC	Ethyl caproate concentration (mol/m <sup>3</sup> )

$I_{Ac}$	Isoamyl acetate concentration (mol/m <sup>3</sup> )
$Y_{EA}$	Ethyl acetate yield per mole sugar fermented (mol/m <sup>3</sup> )
$Y_{EC}$	Yield coefficient for ethyl caproate per mole bio mass growth (mol/m <sup>3</sup> )
$Y_{IAc}$	Yield coefficient for moles isoamyl acetate produced per mole isoamyl alcohol formed (mol/m <sup>3</sup> )
$\mu_{IA}$	Specific rate of isoamyl alcohol formation (h <sup>-1</sup> )
$V_{DK}$	Vicinal diketones concentration (mol/m <sup>3</sup> )
$Y_{V_{DK}}$	Yield coefficient, mole VDK formed per mol biomass growth
$K_{V_{DK}}$	Effective first order rate constant for uptake of VDK (m <sup>3</sup> /mol h)
$AAI$	Acetaldehyde concentration (mol/m <sup>3</sup> )
$Y_{AAI}$	Yield coefficient, moles AAI formed per mole sugar fermented
$K_{AAI}$	Effective first order rate constant for uptake of AAI (m <sup>3</sup> /mol h)
$K_c$	Controller gain
$\tau_i$	Integral time (h)
$SP$	Set point
$GS$	Observed parameter for gain scheduling

